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# Full Length Article

# Predictive models of laminar flame speed in NH<sub>3</sub>/H<sub>2</sub>/O<sub>3</sub>/air mixtures using multi-gene genetic programming under varied fuelling conditions



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#### ARTICLE INFO

#### ABSTRACT

Keywords: NH<sub>3</sub> H<sub>2</sub> Laminar Flame Speed (LFS) Ignition Delay Time (IDT) Ozone (O<sub>3</sub>) Multi-gene genetic programming The primary aim of this study is to develop and validate a novel multi-gene genetic programming approach for accurately predicting Laminar Flame Speed (LFS) in ammonia ( $NH_3$ )/hydrogen ( $H_2$ )/air mixtures, a key aspect in the advancement of carbon-free fuel technologies. Ammonia, particularly when blended with hydrogen, presents significant potential as a carbon-free fuel due to its enhanced reactivity. This research not only investigates the effects of hydrogen concentration, initial temperature, and pressure on LFS and Ignition Delay Time (IDT) but also explores the impact of oxidizing agents like ozone ( $O_3$ ) in augmenting  $NH_3$  combustion. A modified reaction mechanism was implemented and validated through parametric analysis.

Main findings demonstrate that IDT decreases with higher hydrogen concentrations, increased initial temperature, and initial pressure, although the influence of pressure decreases above 10 atm. Conversely, at lower temperatures (below 1200 K) and higher hydrogen concentrations (30 % and 50 %), the dominance of H<sub>2</sub> chemistry can negatively impact initial pressure. LFS increases with higher temperature and hydrogen concentration, but decreases under elevated pressure, with its effect becoming negligible above 5 atm. An optimized equivalence ratio ( $\Phi$ ) range of 1.10 – 1.15 is identified for efficient combustion. Introducing ozone into the oxidizer notably improves LFS in NH<sub>3</sub>/H<sub>2</sub>/air mixtures, with the addition of 0.01 ozone mirroring the effect of a 10 % hydrogen addition under normal conditions.

The study's fundamental contribution is the development of a multi-gene genetic algorithm, showcasing the correlation between predicted LFS values and actual values derived from chemkin simulations. The successful validation of this methodology across various case studies underscores its potential as a robust tool in zero-carbon combustion applications, marking a significant stride in the field.

#### 1. Introduction

The ecological consequences of human actions on the heightened levels of greenhouse gases (GHGs) and the growing concern on the climate change issue have recently prompted research into low or zeroemission alternative solutions as systems employing biofuels or alternative fuels [1–5]. In the current worldwide scenario, the optimization of performance and the reduction of pollutants emissions from aviation transportation are important priorities, a consequence of the spreading concern about the availability of fossil fuel reserves and the focus on finding alternative fuels with high thermal efficiency and clean emission characteristics, as  $H_2$  or  $NH_3$  [6–9].

 $H_2$  is considered a highly promising clean fuel due to its exceptional energy density per unit of mass and absence of carbon-relative pollutant emissions [10]. Currently, most of the hydrogen production process

relies on fossil fuels, which can release carbon dioxide (CO2) as a byproduct, and the overall environmental impact may not be as 'clean' as one might expect. However, there is a growing effort to produce green hydrogen through methods like electrolysis powered by renewable energy sources (i.e. solar, wind, etc.) which has the potential to be a clean and sustainable fuel. Airbus has introduced the "ZEROe" project, with the objective to create in 2035 the first commercial aircraft with zero emissions [11]. For this kind of aircraft, powered by modified gas turbine engines, the purpose is to use liquid H<sub>2</sub>-like fuel [12]. Despite its growing recognition as a fuel, molecular H2 still faces significant limitations due to its high volatility and flammability. These drawbacks include the requirement for specialized infrastructure, as well as the associated costs and safety concerns related to storage and transportation. Nevertheless, the production capacity of H<sub>2</sub> still requires further development in order to entirely replace conventional fossil fuels [13]. In this context, a practical approach to gradually enhance the

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Nomenclature	ML Machine Learning MSE Mean squared error
Acronyms         ANN       Artificial Neural Networks         CHBR       Close Homogeneous Batch Reactor         GA       Genetic Algorithm         CHCc       graphbuse gases	PLFSRPremixed Laminar Flame Speed ReactorRMSERoot-Mean-Squared ErrorSSESum Squared ErrorOPSFOutwardly propagating spherical flame
GHOSgreenhouse gasesGPGenetic ProgrammingHCHydrocarbonsIDTIgnition Delay TimeLFSLaminar Flame SpeedLHVLower Heating ValueLBVLaminar burning velocityMAEMean absolute errorMGGPMulti-gene genetic programming	Symbol $\Phi$ Equivalence ratioPPressure (atm)P_0Ambient pressure (1 atm)R^2Coefficient of determinationTTemperature (K)T_0Ambient Temperature (298 K)

combustion performance and minimize pollutant production in aircraft engines is to blend H<sub>2</sub> with other alternative fuels, for example, methane (CH<sub>4</sub>), and NH<sub>3</sub> [6,14]. Recently, many researchers and companies have moved their interest surrounding NH3 as a carbon-free alternative fuel·NH<sub>3</sub> presents a relatively high energy density of 13 MJ/l. It can be conveniently stored in a liquid state under a pressure of 1.1 MPa at a temperature of 300 K [15]. Furthermore, NH<sub>3</sub> exhibits a Lower Heating Value (LHV), reaching 18.8 MJ/kg. Despite that, due to the high corrosiveness and toxicity of NH3 in real applications, it is essential to utilize rigorous protection and prevention procedures, particularly in real applications for operators. Considering these factors, various recent studies have been conducted to investigate the effects of NH3 on main combustion efficiency, considering various current challenges related to its main combustion parameters, chemical kinetics modeling, and its utilization as fuel in real transport systems [16,17]. However, a significant limitation of NH<sub>3</sub> as a fuel is its notably low combustion intensity. Thus, the improvement of the LFS in practical combustion systems using NH3 represents today an interesting research issue for many scientists [18,19].

Considering the need to combine NH<sub>3</sub> in a mixture, it is important to consider that the ignition energies of NH<sub>3</sub> must be deeply greater than traditional fossil fuels. One of the most common issues due to the low LFS values of NH<sub>3</sub>/air mixtures, combined with the floating effect, is the occurring phenomenon of the propagation of a spherical flame that propagates outwards (OPSF) [20,21]. This results in the loss of its spheric shape and affects the accuracy of experimental measurement methodologies. In these optical, operating parameters, such as  $\Phi$ , IDT, LFS, inlet pressure, and temperature strongly affect the combustion behavior and need optimization to allow for achieving high performance and minimizing the emissions. Numerous experimental studies have explored the improvement of combustion by introducing H<sub>2</sub> as a seed into NH<sub>3</sub>. Lee et al. [22] performed a comprehensive study on laminar premixed H2-added NH3/air flames for H2 production. They focused on examining the combustion features at various  $\Phi$  and for different H<sub>2</sub> fractions within the fuel blend considered. Gotama et al. [23] investigated the Laminar Burning Velocity (LBV) behavior and Markstein length of NH<sub>3</sub>/H<sub>2</sub>/air premixed flames at intermediate H<sub>2</sub> ratio in the binary fuel for different pressures and  $\Phi$ . In order to optimize the modeling of the flame, they developed an optimized mechanism using the measurement of the LFS. Ichikawa et al. [24] examined the LBV and Markstein length of stoichiometric NH<sub>3</sub>/H<sub>2</sub>/air mixtures using the OPSF method at 298 K but with different initial pressures. Han et al. [25] investigated the relation between temperature dependence and the LBV for NH<sub>3</sub>/air flames. In their research, they based their kinetic simulations on different literature mechanisms developed for NH<sub>3</sub> combustion. Lesmana et al [26] conducted an experimental and kinetic modeling study of LFS in mixtures of partially dissociated NH3 in air. In order to

provide LFS, they considered different CHEMKIN modeling including three different reaction mechanisms, the Okafor [27], Otomo [28], and Mathieu and Petersen [29] mechanisms, respectively. The presence of H<sub>2</sub> resulted in an augmentation of crucial radicals such as OH, H, O, and NH<sub>2</sub>, consequently promoting the transformation of NH<sub>2</sub> into NH, HNO, and NNH. This led to a notable upsurge in the LFS. Pessina et al. [30] analyzed the LFS correlations for NH<sub>3</sub>/H<sub>2</sub>/air mixtures at elevated pressures, considering the range of 40–130 bar and high temperatures for the range from 720 K to 1200 K, for various  $\Phi$  (0.4–1.5). They utilized an extensive dataset of chemical kinetics simulations considering various blends of NH<sub>3</sub> and H<sub>2</sub> (ranging from 0 to 100 mol% H<sub>2</sub> in increments of 20).

Many researchers are moving their attention to the effect of oxygen  $(O_2)$  addition in NH<sub>3</sub>/H<sub>2</sub> mixtures. Mei et al. [31] developed a kinetic model to analyze the effects of  $O_2$  enrichment,  $\Phi$ , and initial pressure on the laminar flame evolution of NH<sub>3</sub>. They proved that the  $O_2$  addition can enhance flame propagation and reduce the buoyancy effect. Sreshta et al. [32] examined the laminar flame speeds of NH<sub>3</sub> with  $O_2$ -enriched air (with oxygen content ranging from 21 to 30 vol%) and NH<sub>3</sub>/H<sub>2</sub>-air mixtures (with fuel H<sub>2</sub> content varying from 0 to 30 vol%) at high pressure (1–10 bar) and temperature (298–473 K) values.

Currently, another important challenge is represented by the effects of  $O_3$  addition on combustion features improvement [33].

Ozone is typically generated using corona discharge, ultraviolet radiation, or electrolysis. Corona discharge is the most widely used method for industrial-scale ozone generation, where an electric discharge is used to split oxygen molecules ( $O_2$ ) into individual oxygen atoms [34]. These atoms can then combine with  $O_2$  molecules to form ozone ( $O_3$ ). Recent advancements in this technology focus on enhancing energy efficiency and reducing nitrogen oxide by-products. Integrating ozone into combustion systems requires careful consideration of the ozone's point of entry and the control of its concentration. The method of integration varies based on the combustion system's design and the specific objectives of ozone addition, such as improving flame speed or reducing emissions. Advances in control systems and sensors are crucial for accurately monitoring and adjusting ozone levels in real-time to optimize combustion processes.

Wang et al. [35] investigated the combustion improvement using ozone additives for CH<sub>4</sub>/air flames through the measurement of LBV and the development of kinetic modeling. Chen et al. [36] analyzed the impact of ozone addition on the LBV of premixed flames consisting of NH<sub>3</sub>/(35 %O<sub>2</sub>/65 %N<sub>2</sub>) and NH<sub>3</sub> + CH<sub>4</sub>/C<sub>2</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> + air. Their studies considered a wide range of  $\Phi$ . The introduction of O<sub>3</sub> had notable effects, such as decreasing the ignition energy and increasing the burning velocities of the entire mixture when NH<sub>3</sub> was blended with hydrocarbons (HC). This finding holds significance in the development of NH<sub>3</sub> cofiring mechanisms involving diverse complex fuels, thus validating the feasibility of  $NH_3$  utilization in practical applications. The combined effects of zero-carbon fuel mixture composition and ozone seeding on combustion remain unclear but assume fundamental importance in optimizing and assessing the combustion in a large range of operating conditions. On the other hand, the ozone addition can allow for the reduction of NOx formation in combustion processes [37,38].

In modern research, Machine Learning (ML) methods have gained increasing significance, offering the potential to unravel these intricate interactions and improve our understanding of combustion processes. For instance, ML techniques such as Artificial Neural Networks (ANN) have been successfully applied in studying combustion, flame dynamics, and ignition processes [39,40]. The utilization of ANN offers promising capabilities in non-linear regression, tabulation, and order reduction. This, in turn, enables improved prediction accuracy with reduced memory and CPU-time requirements [41]. Furthermore, ANN can be effectively employed for analyzing experimental measurements [39,42]. Echard et al. [43] compared multiple machine-learning techniques for the calculation of LBV for H<sub>2</sub>-CH<sub>4</sub> mixtures. Also Wan et al. [44] developed an optimal ML model to evaluate the LFS of single hydrocarbon and oxygenated fuel with simple descriptors.

This study analyses the LFS and IDT of the NH<sub>3</sub>/H<sub>2</sub>/air mixtures and investigates the effect of the addition of O<sub>3</sub> in the oxidizer at different  $\Phi$ . With the objective of assessing combustion evolution, a new modeling of LFS and IDT is developed in the CHEMKIN environment [45]. Firstly, the effects of H<sub>2</sub> enrichment (range from 0 % to 50 %) for NH<sub>3</sub>/H<sub>2</sub>/air mixtures are examined and discussed. Secondly, the effects of initial pressure and initial temperature on IDTs and the influence of initial pressure, temperature, and  $\Phi$  on LFS are underlined. Finally, the behavior of LFS for different O<sub>3</sub> content in the oxidizer in terms of mole fraction (0–0.01) of NH<sub>3</sub>/H<sub>2</sub>/air mixtures at various  $\Phi$ , at constant pressure and temperature conditions is analyzed.

This study presents a novel and comprehensive approach to predicting Laminar Flame Speed (LFS) in  $NH_3/H_2/air$  mixtures, marking a significant advancement in the field of carbon-free fuel technologies. At the heart of its innovation is the development of a multi-gene genetic programming method, a groundbreaking tool in the predictive modeling of LFS. This method accurately correlates predicted LFS values with actual values derived from Chemkin simulations, showcasing its robustness and precision.

Focusing on  $NH_3/H_2$  blends, the research delves into a relatively underexplored yet promising area in carbon-free fuels. The study's comprehensive analysis extends beyond standard parameters like hydrogen concentration, initial temperature, and pressure, to include the impact of oxidizing agents such as ozone (O<sub>3</sub>) on combustion dynamics. This approach not only provides a detailed understanding of  $NH_3/H_2/air$  mixtures but also opens up new avenues for optimizing combustion processes.

By implementing and validating a modified reaction mechanism through extensive parametric analysis, the research underscores its commitment to detailed and accurate exploration. This approach ensures that the findings are not only theoretically sound but also practically relevant, particularly in identifying optimized combustion conditions such as the equivalence ratio ( $\Phi$ ) range.

The multi-gene genetic programming approach introduced in this study significantly advances the modeling of Laminar Flame Speed (LFS) in ammonia/hydrogen mixtures, a complex task involving intricate chemical interactions. This method stands in contrast to conventional models such as chemical kinetic modeling, empirical correlations, computational fluid dynamics (CFD), simplified analytical models, and traditional machine learning techniques. Unlike these standard approaches, which may struggle with the non-linear relationships inherent in combustion processes, the multi-gene genetic programming technique proficiently handles these complexities. It offers a more dynamic analysis by integrating NH<sub>3</sub>, H<sub>2</sub>, and O<sub>3</sub>, shedding light on the nuanced effects these components have on LFS.

The incorporation of ozone into NH3 and H2 combustion mixtures

marks a unique aspect of this research. Traditional methods have not extensively explored ozone's role as an oxidizing agent in altering combustion dynamics, particularly in  $NH_3/H_2$  blends. This study's use of multi-gene genetic programming effectively reveals how ozone impacts combustion characteristics, providing novel insights. This approach not only deepens the understanding of combustion processes but also suggests new ways to use ozone in enhancing combustion efficiency and effectiveness.

## 2. Methodology

A comprehensive evaluation of NH<sub>3</sub> combustion mechanisms is performed to modify the mechanism and perform the parametric study. From the comprehensive review of the Mei mechanism [31] is selected for the modification and performs the parametric study because the Mei model more precisely captured the LFS and IDT [31,46] within the experimental uncertainties. In addition, the Mei mechanism was proven to be more precise in predicting NO experimental findings in a jet-stirred reactor [47]. Therefore, the Mei mechanism was chosen as the reference combustion mechanism in this study for further modification and validation. The modified mechanism is validated against various conditions for IDT and LFS, then performed the simulation to study the effect of different key parameters on the LFS and IDT of the NH<sub>3</sub>/H<sub>2</sub>/O<sub>3</sub>/Air mixture. Finally, the study introduces a multi-gene genetic programming technique for predicting LFS in diverse NH<sub>3</sub>/H<sub>2</sub>/O<sub>3</sub>/Air conditions, while taking into account factors such as H2 concentration, initial temperature, and pressure.

#### 2.1. Details of the combustion kinetic mechanism

For NH<sub>3</sub>/H<sub>2</sub>/O<sub>3</sub>/Air mixtures, the combustion mechanism proposed by Mei et al. [31] was modified and validated. This mechanism integrates the H<sub>2</sub> based mechanism from Hashemi et al. [48]. Additionally, a number of chemically termolecular reactions that are essential for the LFS predictions of H<sub>2</sub> (H + O<sub>2</sub> + O/OH/H = products) that were left out of the H<sub>2</sub> mechanism from Hashemi et al. [48] are included in the base H<sub>2</sub> model, the NH<sub>3</sub> sub-mechanism from Shrestha et al. [49].

In the present work the excited species reactions of O (<sup>1</sup>D), O<sub>2</sub> ( $a^{1}\Delta_{g}$ ), which have a positive effect on the LFS introduced by Konnov [50], were added to the base mechanism and also O<sub>3</sub> sub-mechanism reactions present in Table 1 were included from ZH Wang et al. [35] to the base mechanism to investigate the effect of ozone, further details of the mechanism can be found in the [31].

In this study, two different reactor models were employed to analyze the combustion process: the Premixed Laminar Flame Speed Reactor (PLFSR) and the 0D Closed Homogeneous Batch Reactor (CHBR). The

Table 1		
Modified O <sub>3</sub> sub-mechanism integrated into the Mei-Mech	[31]	١.

NO.	Reaction	А	Е	Ν
1.	$O_3+O_2 \rightarrow O_2+O+O_2$	1.54E + 14	23,064	0
2.	$O_3+O \rightarrow O_2+O+O$	2.48E + 15	22,727	0
3.	$\mathrm{O}_3 + \mathrm{N}_2 \rightarrow \mathrm{O}_2 + \mathrm{O} + \mathrm{N}_2$	4.00E + 14	22,667	0
4.	$\mathrm{O}_3 + \mathrm{O}_3 \rightarrow \mathrm{O}_2 + \mathrm{O} + \mathrm{O}_3$	4.40E + 14	23,064	0
5.	$O_2+O+O_2 \rightarrow O_3+O_2$	3.26E + 19	0	$^{-2.1}$
6.	$O_2 + O + O \rightarrow O_3 + O$	2.28E + 15	-1391	-0.5
7.	$O_2+O+N_2 \rightarrow O_3+N_2$	1.60E + 14	-1391	-0.4
8.	$O_2+O+O_3 \rightarrow O_3+O_3$	1.67E + 15	-1391	-0.5
9.	$O_3 + H \rightleftharpoons O + HO_2$	4.52E + 11	0	0
10.	$O_3 + H_2O \rightleftharpoons O_2 + H_2O_2$	6.62E + 01	0	0
11.	$O_3 + NO \rightleftharpoons O_2 + NO_2$	8.43E + 11	2603	0
12.	$O_3 \rightleftharpoons O_2 + O$	4.31E + 14	22,300	0
13.	$O_3 + N \rightleftharpoons O_2 + NO$	6.00E + 07	0	0
14.	$O_3 + O \rightleftharpoons O_2 + O_2$	4.82E + 12	4094	0
15.	$O_3 + H \rightleftharpoons O_2 + OH$	8.430E + 13	934	0
16.	$O_3 + OH \rightleftharpoons O_2 + HO_2$	1.85E + 11	831	0
17.	$\mathrm{O}_3 + \mathrm{HO}_2 \rightleftharpoons \mathrm{OH} + \mathrm{O}_2 + \mathrm{O}_2$	6.62E + 09	994	0

modeling of Laminar Flame Speed (LFS) and Ignition Delay Time (IDT) was conducted using the respective PLFSR and CHBR modules within the CHEMKIN software.

The PLFSR model focuses on a freely propagating premixed flame. This model presumes an adiabatic, one-dimensional flame and utilizes premixed  $\rm NH_3/H_2/N_2/air$  mixtures, integrating multicomponent transport properties. It also operates under the assumption that the impact of radiative heat loss on the flame is negligible, as supported by findings from Nakamura and Shindo (2019) which suggest that the reduction in flame speed due to radiative heat loss is minor and falls within the uncertainty range of standard measurements [51]. The initial conditions for the PLFSR simulations were set at a temperature of 298 K and a pressure of 1 atm. The calculation was performed by solving the governing equations through the Newton iteration algorithm. This method was used to ascertain the eigenvalue of the problem, which effectively corresponds to the laminar burning flux.

The IDT, on the other hand, was estimated using CHEMKIN's Closed Homogeneous Batch Reactor model, which maintains a constant volume. In this context, the simulated IDT is defined as the duration from the start of the simulation to the point where the maximum rate of change in OH concentration is observed. In the CHBR solver, the relative and absolute error tolerance in the ODEs solver is set to be  $1.0e^{-6}$  and  $1.0e^{-12}$ .

All simulations within these models produced grid-independent solutions, ensuring the reliability and accuracy of the computational findings in assessing both LFS and IDT under the specified conditions.

#### 2.2. Validation

To validate the updated combustion mechanism, we utilized both experimental results from studies by Han et al. [52], Ichikawa et al. [24], and Charles et al. [53], as well as simulation results from works by Okafor et al. [27], San Diego et al. [54], and Tian et al. [55]. Specifically, we correlated the Laminar LFS of stoichiometric  $NH_3/H_2/air$  flames across a  $H_2$  blend range from 0 % to 60 %, as illustrated in Fig. 1.

Fig. 1 highlights that the calculated LFS values from the present and San Diego models agree with the experimentally measured data for specific conditions. However, it's notable that the Okafor and Tian model performs well up to a 20 %  $H_2$  concentration but consistently underestimates LFS in all other scenarios.

Figs. 2(a)–(d) show a comparison between the predictions of the present model and other models against experimental IDT data [14] for  $NH_3/H_2$  mixtures at  $\Phi = 1.0$  and pressures of 1.2 atm and 10 atm. In the



**Fig. 1.** LFS of stoichiometric NH<sub>3</sub>/H<sub>2</sub>/air mixtures, as a function of  $x_{H_2}$ , Symbols signify the experiment data, whereas lines show the simulated findings of the current model and prior models at P = 1 atm and T = 298 K.

case of the pure  $NH_3$  mixture (0.04375 $NH_3$ / 0.0328 $IO_2$ / 0.92344Ar), as illustrated in Fig. 2(a) and 2(b), the current model, along with the Zhang Model [56], Otomo Model [28], Mathieu Model [29], and Glabrog Model [57], all yield reasonable predictions for IDTs at 1.2 atm and 10 atm.

The Okafor Model [24] significantly overestimated the IDTs at both 1.2 atm and 10 atm. However, it consistently gives accurate predictions for  $NH_3$  flame speed and NO concentration within the flames. This model is constructed upon the GRI 3.0 model [58] and incorporates  $NH_3$  oxidation kinetics from Tian et al. [55].

The Nakamura Model [59] significantly underestimated the IDT at 10 atm. In agreement with the research conducted by Miller and Bowman [60], NH<sub>3</sub>-related chemistry underwent re-evaluation, drawing from numerous literature investigations. The chemistry of  $N_2H_x$  was based on the research of Konnov et al. [61,62]. It's worth noting that this model exhibited considerable variation in its ability to predict IDT results due to its evaluation limited to species profiles of O<sub>2</sub>, NH<sub>3</sub>, NO, N<sub>2</sub>O, and H<sub>2</sub>O under atmospheric pressure in a weak flame.

The Stagni Model [63] provided faster but significantly underestimated Ignition Delay Times (IDTs) at pressures of 1.2 atm, while it overestimated IDTs at 10 atm and above 1450 K. The chemistry related to HONO/HNO<sub>2</sub> was derived from a theoretical investigation by Chen et al. [64], and the nitrogen chemistry in the model was based on the research by Song et al. [65].

In Figs. 2(c) and (d), with a 30 %  $H_2$  blend in the  $NH_3/H_2$  mixture (0.03322 $NH_3/$  0.01424 $H_2/$ 0.03203 $O_2/$  0.92051Ar), both the present model and the Otomo model reliably predict IDTs at 1.2 atm and 10 atm. The Glarborg Model accurately anticipates IDTs for  $NH_3/H_2$  blends at 1.2 atm but somewhat underestimates them at 10 atm.

The shorter ignition delay time for  $NH_3/H_2$  mixtures at 10 atm compared to 1.2 atm is a result of a combination of factors. These include increased reaction rates due to higher molecular collision frequency, elevated temperatures enhancing chemical reactions, favourable formation of reactive intermediates, reduced heat loss, and improved mixing of reactants due to enhanced molecular interactions. Each of these factors plays a critical role in the complex dynamics of combustion at varying pressures.

#### 3. Results and discussion

#### 3.1. Effect of $H_2$ enrichment in the $NH_3/H_2/air$ mixture on LFS and IDT

LFS is a critical combustion parameter, representing the rate at which the normal flame front advances relative to the unburned mixture.

LFS is frequently used to validate combustion kinetic models, a crucial consideration in the design of practical combustion systems  $NH_3$  is known for its slower flame speed compared to  $H_2$  and hydrocarbon fuels, making it necessary to advance our understanding of how various parameters, including additives, influence  $NH_3$  flame speed to facilitate effective  $NH_3$  oxidation.

Another key element in premixed combustion is the IDT, which represents the duration it takes for a mixture to auto-ignite. Understanding IDT is essential for both theoretical research and for addressing ignition behavior, whether normal or anomalous, in real-world combustion systems. IDT can be determined by observing the time at which a particular species' concentration reaches its peak or when the temperature reaches its inflection point. In this study, IDT is defined as the time at which a specific rate of temperature rise occurs.

The analyzed hydrogen concentration range up to 50 % aims to explore the impact of hydrogen's reactivity on combustion, particularly on ignition and flame stability, while also considering safety concerns like boundary layer flashback. This range reflects practical scenarios, from hydrogen as a minor additive to a major component, in line with the shift towards hydrogen-based energy systems. Similarly, the pressure range of 1 to 30 atm covers conditions from ambient to industrial



Fig. 2. Relationships between the experimental and model-predicted IDTs of stoichiometric NH<sub>3</sub>/H<sub>2</sub> mixtures using present and other models at pressures of 1.2 atm and 10 atm.

settings, crucial for understanding NH3/H2 mixtures' combustion dynamics. This broad pressure spectrum helps identify safe and efficient operational limits and aligns with standard pressures in combustion research, enhancing comparative analysis and insights into these mixtures under various conditions.

Fig. 3 shows the effect of H<sub>2</sub> enrichment and  $\Phi$  on the LFS of NH<sub>3</sub>/ H<sub>2</sub>/air mixture at P = 1 atm and T = 298 K. By increasing the concentration of H<sub>2</sub> in the NH<sub>3</sub>/H<sub>2</sub>/air mixture, the flame speed increases significantly and non-linearly. This behaviour can be due to hydrogen's substantially higher reactivity and flame speed than NH<sub>3</sub>. As NH<sub>3</sub> is steadily replaced by H<sub>2</sub>, the latter takes over as the dominant oxidant.



Fig. 3. Effect of  $H_2$  enrichment and  $\Phi$  of  $NH_3/H_2/air$  mixtures on the LFS at P = 1 atm and T = 298 K.

However, large H<sub>2</sub> concentrations in NH<sub>3</sub>/H<sub>2</sub>/air mixture should be avoided since hydrogen's strong reactivity might cause boundary layer flashback [66]. Furthermore, the flame speed grows consistently at fuellean conditions, peaks when the  $\Phi$  is around 1.1–1.15, and subsequently decreases at fuel-rich conditions.

In the presence of 40 % and 50 %  $H_2$  in the mixture, the maximum LFS reaches approximately 29 cm/s and 44 cm/s, respectively, at  $\Phi$  of 1.1. To provide context, pure methane burns at a premixed flame speed of about 37 cm/s [27] under identical conditions, while pure  $H_2$  burns at a premixed flame speed of above 200 cm/s [24]. This suggests that using an NH<sub>3</sub>/H<sub>2</sub>/air mixture with an  $\Phi$  of 1.1–1.15 is a viable approach to achieve stable combustion in the combustor.

Fig. 4 shows the IDT as a function of  $H_2$  concentration in  $NH_3/H_2/air$  mixtures at 1 atm,  $\Phi = 1.0$ , and temperatures ranging from 1000 K to 2000 K. As evident in Fig. 4, IDT decreases as the  $H_2$  concentration in the mixture increases from 0 % to 50 %. Specifically, when the  $H_2$  concentration in the mixture approaches 50 %, the IDT reduces from approximately 2222 ms to about 1.1 ms at 1000 K and from around 3 ms to roughly 0.05 ms at 1500 K. This indicates that incorporating a more reactive fuel component into  $NH_3$  significantly reduces the IDT, which is advantageous for achieving robust ignition.

### 3.2. Effect of initial pressure on LFS and IDT of $NH_3/H_2/air$ mixture

Fig. 5 illustrates the impact of the initial pressure of  $NH_3/H_2/air$  mixtures on the LFS at 298 K and various  $\Phi$ . With increasing initial pressure, the laminar flame speed decreases. Higher pressures result in a thicker flame and a slower burning speed. The influence of initial pressure is more pronounced at pressures up to 5 atm in all scenarios, while the effect diminishes at higher pressures.

In the case of pure NH<sub>3</sub>/air case (H<sub>2</sub> = 0 %) at  $\Phi$  = 1 and  $\Phi$  = 1.1 the LFS decreases from 6.5 cm/s to 4.4 cm/s and 8.1 cm/s to 5.8 cm/s when pressure decreases from 1 atm to 5 atm, whereas it decreases from 4.4



Fig. 4. Effect of  $H_2$  enrichment of  $NH_3/H_2/air$  mixtures on IDT at  $\Phi = 1$ , P = 1 atm.

cm/s to 3.7 cm/s and 5.8 cm/s to 5 cm/s when pressure decreases from 5 atm to 10 atm, respectively.

In the case of 30 % of H<sub>2</sub> in the mixture at  $\Phi=1$  and  $\Phi=1.1$  the LFS decreases from 16.9 cm/s to 9.7 cm/s and 19 to 12.1 cm/s when pressure decreases from 1 atm to 5 atm, whereas it decreases from 9.7 cm/s to 7.9 cm/s and 12.1 cm/s to 10 cm/s when pressure decreases from 5 atm to 10 atm, respectively. This means that the LFS is less sensitive to initial pressure under high-pressure situations, which are more common in engine operating settings.

Figs. 6 (a)–(d) demonstrate the impact of initial pressure (ranging from 1 atm to 30 atm) on the IDT of stoichiometric  $NH_3/H_2/air$  mixtures with  $H_2$  concentrations of 0, 10, 30, and 50 %, across temperatures from

1000 K to 2000 K. As depicted in Figs. 6 (a) and (b), for mixtures containing 0 % and 10 % H<sub>2</sub>, an increase in initial pressure shortens the IDT within the temperature range of 1000 K to 2000 K. However, the rate of reduction diminishes as the initial pressure continues to rise. When the initial pressure exceeds 10 atm, the influence of initial pressure on ignition delay becomes marginal.

The initial pressure demonstrates a negative effect on the IDT in the temperature range of 1000 K to 1100 K for the cases of 30 % and 50 % H<sub>2</sub> in the stoichiometric NH<sub>3</sub>/H<sub>2</sub>/air mixtures, as indicated in Figs. 6(c) and (d). In the case of 30 % and 50 % H<sub>2</sub> in the mixture, the IDTs can be shortened only at high temperatures (T > 1200 K), whereas at lower temperatures, the IDTs can become significantly longer.

The impact of initial pressure on the IDT is observed to have a negative effect within the temperature range of 1000 K to 1100 K for the scenarios involving 30 % and 50 % H<sub>2</sub> in the stoichiometric NH<sub>3</sub>/H<sub>2</sub>/air mixtures, as depicted in Figs. 6(c) and (d). It's worth noting that for these blends the reduction in IDTs is only significant at high temperatures (T > 1200 K), while at lower temperatures, the IDTs can become notably longer.

The negative pressure dependence indicated above was also studied in the literature with respect to the ignition delays of H<sub>2</sub>-enriched hydrocarbons [36,67-71]. When the H<sub>2</sub> concentration is sufficiently high, the H<sub>2</sub> chemistry dominates the ignition delays of the dual mixture [69-71].

#### 3.3. Effect of initial temperature on LFS of NH<sub>3</sub>/H<sub>2</sub>/air mixture

Fig. 7 shows that as the initial temperature of the mixture rises, the LFS also increases, and this pattern is consistent across all cases, with the highest value falling within the  $\Phi$  range of 1.1–1.15. At a  $\Phi$  of 1.15, the LFS increases from approximately 8.1 cm/s to about 20 cm/s when the initial temperature of the mixture is raised from 298 K to 473 K.

 $\rm NH_3/H_2/air$  mixtures follow the same behaviour as  $\rm NH_3/air$  mixtures in increasing the initial temperature, and the maximum value for LFS



Fig. 5. Effect of initial pressure on LFS of NH<sub>3</sub>/H<sub>2</sub>/air mixtures at different  $\Phi$  a)  $\Phi$  = 0.8b)  $\Phi$  = 0.9c)  $\Phi$  = 1.0 d)  $\Phi$  = 1.1 and P = 1 atm, T = 298 K.



Fig. 6. Effect of initial pressure on IDT of stoichiometric  $NH_3/H_2/air$  mixtures a)  $H_2 = 0$  %, b)  $H_2 = 10$  %, c)  $H_2 = 30$  %, d)  $H_2 = 50$  % at the temperature ranging from 1000 K to 2000 K.



Fig. 7. Effect of initial temperature and  $\Phi$  on LFS of NH<sub>3</sub>/air mixtures at P = 1 atm.

lies in the equivalence range of 1.1–1.15, as shown in Figs. 8 (a)–(d). For H<sub>2</sub> blends of 5 % (Fig. 8a), 10 % (Fig. 8b), 30 % (Fig. 8c), and 50 % (Fig. 8d), the LFS increases at  $\phi = 1.15$ , and it rises from 9.4 cm/s to 22 cm/s, 10.5 cm/s to 24.5 cm/s, 19 cm/s to 43 cm/s, and 43.5 cm/s to 95.4 cm/s for each respective H<sub>2</sub> blend.

The distinctive properties of  $H_2$  play a key role in accelerating the laminar flame speed, especially when it's part of a mixture with NH<sub>3</sub>. One of the most achieving features of hydrogen is its high reactivity. Thanks to its wide flammability range and relatively low ignition

energy,  $H_2$  sets the stage for rapid chemical reactions. This becomes particularly evident in its interaction with other gases like ammonia, where its presence significantly speeds the combustion process, thereby increasing the speed at which the flame front propagates.

Moreover, hydrogen's remarkably low molecular weight marks it as one of the lightest gases available. This characteristic bestows upon  $H_2$  a superior diffusivity, enabling its molecules to move and intermingle with air or other oxidizers much more rapidly than heavier molecules. This efficient mixing is crucial; it enhances the overall combustion process, facilitating a quicker advancement of the flame.

Another key aspect is hydrogen's high heat of combustion. When  $H_2$  burns, it releases a considerable amount of energy, elevating the temperature of the flame. It's a well-known fact that higher flame temperatures are synonymous with increased reaction rates, which in turn, speed up the flame's progression.

Additionally, the activation energy required for  $H_2$  combustion is notably lower compared to many other fuels. This lower threshold means that the necessary reactions for combustion are more easily initiated and proceed at a faster pace, further boosting the flame speed.

Hydrogen's role becomes even more pronounced when considering its effect on turbulent mixing. The addition of hydrogen to the mixture can significantly alter the physical dynamics of turbulence. This enhanced turbulence, in turn, leads to a more efficient rate of heat and mass transfer, all contributing to a faster-moving flame front.

Lastly, the very presence of  $H_2$  in an  $NH_3/H_2$  mix alters the traditional combustion mechanisms. Hydrogen actively engages in chainbranching reactions, a critical component in the propagation of flames. These reactions facilitate a more effective and efficient combustion process, ultimately leading to an increase in the laminar flame speed.



Fig. 8. Effect of initial temperature and  $\phi$  on LFS at different H<sub>2</sub> concentrations a) H<sub>2</sub> = 5 %, b) H<sub>2</sub> = 10 %, c) H<sub>2</sub> = 30 %, d) H<sub>2</sub> = 50 % at P = 1 atm.



Fig. 9. Effect of  $O_3$  and  $\phi$  on LFS of  $NH_3/H_2/air$  mixtures at different  $H_2$  concentrations a)  $H_2 = 0$  %, b)  $H_2 = 10$  %, c)  $H_2 = 20$  %, d)  $H_2 = 30$  % and P = 1 atm, T = 298 K.

#### 3.4. Effect of O<sub>3</sub> on LFS of NH<sub>3</sub>/H<sub>2</sub>/air mixture

Previous research has shown that adding O<sub>3</sub> to hydrocarbon fuels improves LFS. Wang et al. [35] used a heat flux burner and found that injecting 3730 ppm O<sub>3</sub> at stoichiometric conditions increased the LFS of CH<sub>4</sub>/air by 3.5 %. X Gao et al.[72] investigated the effect of O<sub>3</sub> on LFS experimentally and numerically utilizing three fuels, CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, and C<sub>3</sub>H<sub>8</sub>, over a wide pressure range and found that for a stoichiometric CH<sub>4</sub>/air mixture with 6334 ppm O<sub>3</sub> addition, the improvement in the measured flame speed increased from 7.7 % at atmospheric pressure to 11 % at 2.5 atm. Ombrello et al. [73] showed a 4 % increase in LFS of C<sub>3</sub>H<sub>8</sub> /air in stoichiometric lifted flames. Weng et al. [74] reported a stronger effect in fuel-rich mixes than in stoichiometric mixtures. The improvement in LFS is intimately linked to the chemistry of ozone, particularly the fast exothermic ozonolysis reactions that involve unsaturated hydrocarbons and the decomposition of O<sub>3</sub> to form atomic oxygen. However, no such investigations on NH<sub>3</sub>/H<sub>2</sub>/air mixtures with O3 addition have been conducted.

Fig. 9 shows the effect of the  $O_3$  concentration in the oxidizer in terms of mole fraction (0 – 0.01) on the LFS at various  $H_2$  concentrations (0–30%) and  $\phi$  of  $NH_3/H_2/air$  mixtures at a pressure equal to 1 atm, and temperature equal to 298 K.

Ozone generation using plasma discharge [34], typically yields ozone concentrations that can vary significantly depending on various factors such as the type of plasma generator, discharge power, and gas flow rates. These concentrations usually range from a few parts per million (ppm) to several thousand ppm. The range of 0–0.01 mol fraction considered in the present study likely corresponds to this practical and achievable spectrum for plasma discharge systems, making it relevant for experimental and real-world applications.

Furthermore the range is comparable to those used in other research involving different fuel/air mixture, i.e. CH<sub>4</sub>/air [35,72].

Enhancing the oxidizer by increasing the concentration of  $O_3$  from 0 to 0.01 markedly improves the laminar flame speed (LFS) across all cases, an observation that underscores the critical role of ozone in the combustion process. This enhancement can be attributed to the conversion of ozone into oxygen, which effectively raises the concentration of atomic oxygen (O). This additional oxygen plays a significant role in the chemical processes involving ammonia, leading to an increased rate of ammonia oxidation and overall improvement in combustion efficiency.

The impact of this ozone enhancement on the LFS is most notable within a specific range of equivalence ratios ( $\Phi$ ), particularly between 1.1 and 1.15. In this range, the LFS demonstrates its peak values, reflecting the optimum conditions for combustion. For instance, in the absence of hydrogen (pure NH<sub>3</sub>/air mixture), the LFS sees an increase from 8.1 cm/s to 10.28 cm/s as shown in Fig. 10. Similarly, with incremental additions of H<sub>2</sub> — 10 %, 20 %, and 30 % — the LFS values show a corresponding rise from 10.5 cm/s to 13.04 cm/s, 13.8 cm/s to 17.07 cm/s, and 18.99 cm/s to 23.69 cm/s, respectively. These increases highlight the profound effect of integrating ozone into the oxidizer mix.

Furthermore, the role of hydrogen in this context cannot be overstated. Hydrogen's unique characteristics, including its high reactivity, minimal weight, substantial energy output, reduced requirement for activation energy, and its significant impact on combustion dynamics, collectively contribute to its status as a transformative element in combustion processes. When H<sub>2</sub> is combined with NH<sub>3</sub>, it significantly enhances the combustion efficiency, which is further augmented with each increase in ozone concentration. This synergy between H<sub>2</sub> and O<sub>3</sub> in the presence of NH<sub>3</sub> leads to a notable acceleration in the flame speed, demonstrating the intricate interplay of these components in optimizing combustion.

#### 4. Genetic programming

In this study, multi-gene genetic programming (GP) was employed to



Fig. 10. Effect of ozone in the oxidizer in terms of mole fraction on maximum LFS of  $NH_3/H_2/air$  at normal conditions.

accurately predict the laminar flame speed under various fuel mixture conditions.

Genetic Programming (GP) and Genetic Algorithm (GA) are both subfields of evolutionary computation (EA), but they have distinct characteristics and applications.

The main difference between genetic algorithms (GAs) and genetic programming (GP) lies in the core nature of their components. GAs represent individuals as unchangeable symbolic strings with fixed dimensions, similar to chromosomes. In contrast, in GP, individuals manifest as a wide array of non-linear entities, featuring variations in both magnitude and complex configuration. These entities dynamically evolve, resulting in intricate parse trees. This innovative approach opens new dimensions for evolutionary exploration [75].

In genetic programming (GP), key components include arithmetic functions, decision variables, and evolutionary operators like reproduction, crossover, and mutation. These elements form initial symbolic expressions, establishing the algorithm's initial population. The process uses a tree-based method combining arithmetic functions with decision variables.

During iterations, the algorithm refines this population based on fitness, using genetic operators. Reproduction selects the fittest individuals, crossover mixes parts of two 'parent' individuals to create 'offspring,' and mutation introduces random changes. This cycle continues until reaching a predefined endpoint, such as a maximum number of generations or an error threshold.

In the reproduction phase of genetic programming, the bestperforming segment of the population is retained to form a new generation through genetic manipulations. During crossover, pairs of individuals are selected and combined at random points in their structure, creating new 'offspring'. The population is then updated with these new individuals. This process repeats iteratively until a termination criterion, like a maximum number of generations or an error threshold, is met.

GP stands as a symbolic modeling technique of the metaheuristic kind, which forges problem-solving equations guided by the principles of Darwinian natural selection, specifically the concept of 'survival of the fittest' [76]. Presented below is the fundamental structure of the anticipated process model: (Equation (1):

$$y = f(X, \beta) \tag{1}$$

the symbol "f' signifies a non-linear function, characterized by parameters articulated through a P-dimensional vector, denoted as  $(\beta[\beta_1, \beta_2, ..., \beta_K]^P)$ . When presented with input and output variables, the GP

Table 2 GP run parameters

or run purumeters.	
Run parameter	Value
Population size	300
Max. generations	500
Generations elapsed	500
Input variables	2
Nodes	40
Training instances	3992
Tournament size	10
Rain Elite fraction	0.15
Lexicographic selection pressure	On
Probability of pareto tournament	0
Max. genes	4
Crossover probability	0.84

algorithm dynamically adjusts its functional configuration and parameter vector  $\beta$  to align with the provided dataset.

Multi-gene genetic programming (MGGP) is a novel approach that enhances the precision of Genetic Programming by using multiple trees to represent a model, as opposed to the single tree used in conventional GP. Each tree in MGGP, akin to a mathematical expression, contributes to a more intricate and accurate prediction of the output. [77].

MGGP differs from conventional GP by allowing users to precisely set key parameters, like the maximum number of genes and their depth. This control significantly influences the complexity and efficiency of the resulting model, with studies showing MGGP's enhanced accuracy and computational efficiency over traditional GP. [78].

The development of the GP-based model was facilitated by the use of the open-source GPTIPS toolkit and custom-coded subroutines in MATLAB 2019a [76]. The framework adopted in this study encompassed the utilization of the Root-Mean-Squared Error (RMSE) between actual and predicted outcomes as the designated fitness function. The effort was dedicated to minimizing the RMSE value, thereby optimizing the model's predictive performance.

It's important to note that this method is both non-parametric, as it doesn't rely on a predefined functional model, and data-driven, as the optimal model is exclusively determined by the data.

The GP was used to perform a multi-gene genetic programming approach, enabling accurate prediction of laminar flame speed. This prediction was achieved using the dataset from Chemkin, encompassing data for freely propagating laminar flames.

A crucial aspect of our approach was the data partitioning strategy. After extensive testing with various split ratios for dividing the dataset into training and testing sets, it was determined that an 80:20 split ratio is the most effective for the model in question. This decision was reached following a series of experiments where different ratios, ranging from 60:40 to 90:10, were evaluated. In each instance, the model's performance was closely monitored, with particular attention paid to its ability to generalize on unseen data while avoiding overfitting. The choice of the 80:20 split emerged as the optimal balance, ensuring sufficient training data to learn effectively while providing a substantial testing set for a reliable evaluation of the model's performance.

Table 2 provides an overview of the model parameters.Different conditions have been analyzed, as follows:

- $\bullet$  Case A: Pure ammonia at ambient conditions (298 K, 1 atm) and different  $\varphi.$
- Case B: Pure ammonia at different  $\phi$ , ambient pressure and 298 K.
- $\bullet$  Case C: Blend NH\_3/H2 at different  $\varphi$  and H2 fraction at ambient conditions (298 K, 1 atm).

- Case D: Blend  $NH_3/H_2$  at different  $\phi$  and ambient pressure at 298 K.
- $\bullet$  Case E: Blend  $NH_3/H_2$  at different  $\varphi,$  ambient pressure and temperature.
- Case F: Blend  $NH_3/H_2$  at different  $\phi$ , with air and  $O_3$  addition.
- Case G: Blend  $NH_3/H_2$  at different  $\phi$ ,  $H_2$ , pressure, temperature, and with air and  $O_3$  addition.

Case A: Pure ammonia at ambient conditions (298 K, 1 atm) and different  $\phi$ .

The following equation was selected as the best model for the LFS in the case of pure ammonia at ambient conditions:

$$LFS = \phi^* 3.26e^2 + exp(-\phi^3)^* 3.23e^2 - exp(-\phi^6)^* 4.64e^1 - \phi^3 * log(\phi)^* 5.41e^1 - 4.21e^2$$

In the study, the effectiveness of the multi-gene genetic programming model is quantitatively showcased in Table 3, which details the model's performance metrics during both the training and testing phases. Additionally, Fig. 11a graphically represents the correlation between measured and predicted values of laminar flame speed (LFS) for the test dataset. The strength of this correlation is quantified by the coefficient of determination, R2, which is remarkably high in both examined scenarios, underscoring the model's accuracy.

Specifically, for Case A, which examines pure ammonia at ambient conditions (298 K, 1 atm) across various equivalence ratios ( $\Phi$ ), the R2 value reaches an impressive 0.9975. This near-perfect correlation indicates an extremely high level of precision in the model's predictions under these standard environmental conditions.

On the other hand, Case B, which involves pure ammonia with varying  $\Phi$  at a constant temperature of 298 K and ambient pressure, shows a slightly lower, yet still significantly high,  $R^2$  value of 0.990. This indicates that while there is a slight decrease in predictive accuracy compared to Case A, the model still maintains a strong predictive capability in this scenario.

These R2 values, particularly the exceptionally high value in Case A, demonstrate the robustness and reliability of the multi-gene genetic programming approach in predicting LFS under varying conditions. The minor difference in the R2 values between the two cases also provides valuable insights into the model's performance under different sets of combustion conditions, highlighting its comprehensive applicability in combustion research.

Case B: Pure ammonia at different  $\phi$ , pressure and 298 K.

The optimal model chosen for the LFS with pure  $NH_3/air$  mixtures at different  $\Phi$  and pressure and ambient temperature is represented by the following equation:

$$\begin{split} LFS &= \phi^{*}5.42 - exp(\phi^{*}6.36 + \phi^{2}*3.0)^{*}3.35e^{-5} + exp(exp((P/P0)^{*} \\ &- 7.58e^{-1})^{*} - 1.0)^{*}3.64 + (\phi^{2}*1.23e^{1})/abs(\phi \\ &+ (P/P_{0})) + \phi^{5}*2.71 - 6.13 \end{split}$$

Table 3 displays the metrics obtained from both the training and testing phases. Additionally, Fig. 11b provides a visual representation of the comparison between the LFS values that were found with chemkin and those that were predicted specifically for the test dataset by GP. The results distinctly indicate a robust association between the forecasted information generated by the multi-gene model and the target data.

Case C: Blend  $NH_3/H_2$  at different  $\phi$  and  $H_2$  fraction at ambient conditions (298 K, 1 atm).

The laminar flame speed for freely propagating laminar flames at 298 K and 1 atm and different  $\phi$  and H<sub>2</sub> content (from 0 to 100) was found. The best model is given by the following equation:

$$LFS = 315.0tanh(\phi^{2}) + 419.0(2.0\phi + X_{H2})^{1/2} - 416.0(\phi + X_{H2} - 1.0exp(-1.0\phi))^{1/2} + (1.3e^{16}X_{H2} + 1.64e^{16})/(3.52e^{13}\phi + 1.76e^{13}X_{H2} + 1.74e^{13}) - 813.0(1.5e^{13}A_{H2} + 1.54e^{13}) - 813.0(1$$

#### Table 3

Metrics for LFS Predictions for different conditions.

Metric	CASE A	CASE B	CASE C	CASE D	CASE E	CASE F	CASE G
Training							
R <sup>2</sup>	0.99773	0.99134	0.99976	0.99638	0.98794	0.98061	0.98647
RMSE	0.071081	0.20848	0.70069	2.7601	11.0105	18.1117	15.0216
MAE	0.059015	0.1278	0.4469	1.865	8.199	12.6419	10.771
SSE	3.8399	32.9902	1959.918	24896.63	165359.2	1177969.46	810304.1037
Max. abs. Error	0.16079	4.0464	6.1563	27.5005	85.0807	116.0078	200.9182
MSE	0.005053	0.043465	0.49096	7.6183	121.2311	328.0338	225.6486
Test							
R <sup>2</sup>	0.9975	0.98993	0.99972	0.99689	0.98713	0.97751	0.98676
RMSE	0.070845	0.24475	0.75518	2.5729	10.3409	18.7693	14.8683
MAE	0.058827	0.13984	0.45876	1.7811	7.6527	13.2974	10.6677
SSE	0.95863	11.3812	569.7228	5414.809	36571.68	316352.28	198517.7684
Max. abs. error	0.15918	2.6618	6.3697	17.842	54.3409	123.0659	102.8528
MSE	0.005019	0.059901	0.57029	6.6196	106.9347	352.2854	221.0666



**Fig. 11.** Target (Chemkin) versus predicted (multigene GP) data for the LFS for  $NH_3$ / air mixtures at: a) different  $\Phi$  and P = 1 atm T = 298 K; b) at different  $\Phi$  and pressure at T = 298 K.



Fig. 12. Target (Chemkin) versus predicted (multigene GP) data for the LFS for  $NH_3/H_2/air$  mixtures at: a) different  $\Phi$  and  $H_2$  mass fraction at 298 K and 1 atm, b) different  $\Phi$ ,  $H_2$  mass fraction and pressure at 298 K.

Where  $X_{\rm H2}$  is the mass fraction ranging from 0 for pure  $NH_3$  to 100 for pure  $H_2.$ 

through chemkin and the ones predicted exclusively for the test dataset

for pure H<sub>2</sub>. Similar to the previous comparisons, the predictive performance in this case is also favorable. Table 3 presents the metrics acquired during both the training and testing stages. Furthermore, Fig. 12a offers a graphical depiction of the contrast between the LFS values obtained  $Case D: Blend NH_3/H_2 a$ The laminar flame speed laminar flames assuming to pressure range of 1 atm to various  $\phi$  and H<sub>2</sub> concent

using GP. The outcomes clearly affirm a strong correlation between the projected insights produced by the multi-gene model and the intended target data.

# Case D: Blend $NH_3/H_2$ at different $\phi$ and pressure at 298 K.

The laminar flame speed has been investigated for freely propagating laminar flames assuming temperatures from 298 K to 500 K and a pressure range of 1 atm to 30 atm. These investigations encompass various  $\phi$  and H<sub>2</sub> concentrations ranging from 0 to 100. Among the different models examined, the most effective one is depicted by the

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# subsequent equation:

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 $LFS = (5.3e^{15}X_{H2}tanh(log(\phi)))/(1.76e13X_{H2} + 8.8e^{12}P/P_0) - (5.23e^{15}(P/P_0)^{1/2})/(8.8e^{12}(P/P_0) + (8.8e^{12}X_{H2})/\phi + 8.8e^{12}(P/P_0)^{1/2}) - 90.6log((P/P_0) + 6.9) + (132.0X_{H2}(x_3 - 2.03))/((X_{H2} + 8.51)(X_{H2} + (P/P_0) + 10.0)) + 407.0$ 

Where  $X_{H2}$  is the mass fraction ranging from 0 for pure  $NH_3$  to 100 for pure  $H_2$  and  $P/P_0$  is the ratio between the pressure and the ambient pressure at 1 atm.

The predictive performance remains promising in this instance as well. Table 3 showcases the metrics gathered from both the training and testing phases. Additionally, Fig. 12b provides a visual representation highlighting the distinction between the target LFS values and those exclusively forecasted for the test dataset utilizing GP. The results undeniably underscore a robust correlation between the anticipated insights generated by the multi-gene model and the desired target data.

Case E: Blend NH<sub>3</sub>/H<sub>2</sub> at different  $\phi$ , ambient pressure and temperature.

The laminar flame speed has been investigated for freely propagating laminar flames assuming temperatures from 298 K to 500 K and a pressure range of 1 atm to 30 atm. These investigations encompass various  $\Phi$  and H<sub>2</sub> concentrations ranging from 0 to 100. Among the different models examined, the most effective one is depicted by the subsequent equation:

$$\begin{split} LFS &= 0.246 log(\phi^3) (log((P/P_0)) - 1.0\phi^3) (X_{H2} + X_{H2}/(P/P_0) + 15.8) \\ &- 0.556 \phi^3 (T/T_0)^2 (\phi + X_{H2}) - 31.0 log((P/P_0)/(T/T_0)) \\ &+ 31.0\phi^2 (T/T_0)^2 log(X_{H2}) + 1.34\phi^2 (T/T_0)^2 log(X_{H2}) ((T/T_0) + 4.77)^{1/2} \\ &\left( log(X_{H2}) - 1.0(P/P_0)^{1/2} \right) + 105.0 \end{split}$$

Where  $X_{H2}$  is the mass fraction ranging from 0 for pure NH<sub>3</sub> to 100 for pure H<sub>2</sub>, P/P<sub>0</sub> is the ratio between the pressure and 1 atm and T/T<sub>0</sub> is the ratio between the temperature and 298 K.

The predictive capability continues to show promise in this scenario as well. Table 3 presents the metrics acquired during both the training and testing stages. Furthermore, Fig. 13 underlines the good agreement between the target LFS values and those predicted for the test dataset using GP.

Fig. 14 presents a detailed surface plot that demonstrates how the laminar flame speed (LFS) varies for different  $NH_3/H_2$  blends under a



Fig. 13. Target (Chemkin) versus predicted (multigene GP) data for the LFS for  $NH_3/$   $H_2/air$  mixtures at different  $\Phi$ ,  $H_2$  mass fraction, pressure, and temperature.



Fig. 14. LFS predicted for  $NH_3/H_2/air$  mixtures at different  $\Phi$ ,  $H_2$  mass fraction, pressure, and temperature.

variety of operational conditions, as predicted by our model. This figure effectively highlights the complex relationship between the flame behavior and various operational factors such as pressure, temperature, fuel-to-air ratio, and hydrogen concentration.

In the figure, the first plot at the top depicts the Laminar Flame Speed (LFS) under specific conditions where the pressure is fixed at 1 atm and the temperature at 298 K. In this plot, the variables being explored are the fuel—air ratio and the hydrogen fraction.

The second plot, maintaining a constant pressure of 1 atm and a fuel-air ratio of 1, varies the temperature and the hydrogen fraction. This plot is designed to show the impact of temperature changes and varying hydrogen concentrations on the LFS, while keeping the pressure and fuel-air ratio constant. It provides insights into how temperature and hydrogen content interact and affect the combustion dynamics in the given conditions. Finally, the third plot fixes the temperature at 298 K and the fuel-air ratio at 1, while varying the pressure and the hydrogen fraction. This plot examines the influence of different pressure levels and hydrogen concentrations on the LFS, with all other variables held steady. It helps in understanding the relationship between pressure variations, hydrogen content, and their combined effect on the Laminar Flame Speed in the context of the specified temperature and fuel-air ratio.

Notably, ammonia (NH<sub>3</sub>) typically exhibits moderate laminar burning velocities, particularly when contrasted with the faster combustion rates of hydrogen (H<sub>2</sub>). The integration of H<sub>2</sub> into NH<sub>3</sub>, however, leads to a noticeable enhancement in the LFS of NH<sub>3</sub>/air mixtures. This increase in LFS is more pronounced at higher H<sub>2</sub> concentrations. The reason behind this trend can be partly attributed to the increased importance of the H<sub>2</sub>-chemistry, especially its chain branching reactions [79], and its inherently high reactivity [80].

This pattern aligns with findings in similar studies, such as those conducted by Di Sarli et al. [81] and Mitu et al. [82], which explored  $H_2/$  CH<sub>4</sub>/air mixtures. These studies also observed comparable trends in LFS enhancement with varying  $H_2$  concentrations, further validating the patterns seen in our NH<sub>3</sub>/H<sub>2</sub> blends. The surface plot in Fig. 14 not only corroborates these findings but also provides a visual representation of how changes in  $H_2$  concentration and other operational variables intricately influence the combustion characteristics of NH<sub>3</sub>/H<sub>2</sub>/air mixtures.

Case F: Blend NH\_3/ H\_2/ O\_3/air at different  $\phi,$  and O\_3 addition at ambient conditions.

The laminar flame speed for freely propagating laminar flames was calculated at 298 K and 1 bar for various  $\Phi$  and H<sub>2</sub> contents (ranging from 0 to 100), including cases where ozone was introduced. The optimal model identified through Genetic Programming is represented by the following equation:

$$LFS = 4149.51^{*}X_{O3} + 200.0^{*}\phi + (4150.51^{*}X_{O3} + 0.77^{*}\phi^{*}X_{H2}/((-X_{O3} + X_{H2})^{*}(200.0^{*}\phi + 0.386)^{*}(-\phi + X_{H2} + 0.996)^{*}(X_{O3}^{*}\phi + X_{H2} - 0.507 + 0.0572^{*}X_{H2}^{2}/\phi)) + 201.0^{*}\phi - X_{H2} + 189.141 + (5368.05^{*}X_{O3}^{*}\phi^{*}(\phi - X_{H2}) + X_{O3} + 189.14)/(-X_{H2} - 0.52))/(-X_{H2} - 0.52)$$

Where  $X_{H2}$  is the mass fraction ranging from 0 for pure NH<sub>3</sub> to 100 for pure H<sub>2</sub>,  $X_{O3}$  is the mass fraction of O<sub>3</sub> with respect to the total oxides fraction ranging from 0 to 0.03.

Metrics obtained in the training and testing stages are presented in Table 3. In this case, as well, the predictive capability continues to show promise. Furthermore, Fig. 15 provides a graphical representation of the difference between the LFS values that were predicted specifically for the test dataset using GP and those that were produced via chemkin. The outcomes clearly confirm a significant relationship between the multigene model's predicted insights and the desired target data.

Case G: Blend NH<sub>3</sub>/H<sub>2</sub> at different  $\phi$ , H<sub>2</sub>, pressure, temperature, and with air and O<sub>3</sub> addition.

The laminar flame speed has been investigated for freely propagating



Fig. 15. Target (Chemkin) data versus predicted (multigene GP) data for the LFS for  $NH_3/H_2/O_3/air$  mixtures at different  $\phi$ ,  $x_{H2}$ , and  $x_{O3}$ .

laminar flames assuming temperatures from 300 K to 500 K, pressure range of 1 atm to 30 atm, and  $O_3$  range of 0–0.03 in the oxidizer. These investigations encompass various  $\Phi$  and  $H_2$  concentrations ranging from 0 to 100. The optimal model identified through Genetic Programming is represented by the following equation:

$$LFS = 10.6exp(2.0X_{O3} + T/T_0)(2.0X_{O3} + T/T_0 - 1.0P/P_0^{1/2}) + (0.113P/P_0^{1/2}(P/P_0 - 1.0X_{H2}T/T_0))/\phi - 694.0X_{O3}\phi(X_{O3} - 1.0T/T_0)(2.0X_{O3} + T/T_0 + exp(-1.0\phi) + log(X_{H2})) + 27.8\phi T/T_0 log(3.03X_{H2})(T/T_0 - 1.0exp(-1.0X_{H2})) + 70.6$$

Where  $X_{H2}$  is the mass fraction ranging from 0 for pure  $NH_3$  to 100 for pure  $H_2$ ,  $X_{O3}$  is the mass fraction of  $O_3$  with respect to the total oxides fraction ranging from 0 to 0.03. and  $P/P_0$  is the ratio between the pressure and 1 atm and  $T/T_0$  is the ratio between the temperature and 298 K.

Fig. 16 clearly demonstrates the strong agreement between the target LFS values and those predicted for the test dataset using GP.



**Fig. 16.** Target versus predicted (multigene GP) data for the LFS for  $NH_3/H_2/$  air mixtures at different  $\Phi$ ,  $H_2$  mass fraction, pressure, temperature, and with  $O_2/air$  mixture as the oxidizer.



Fig. 17. LFS for NH<sub>3</sub>/ H<sub>2</sub>/O<sub>3</sub>/air mixtures at a) different initial temperature and  $x_{O3}$ ,  $\phi = 1$ ,  $x_{H2} = 30$ , P = 1 atm b) different  $x_{O3}$  and  $\phi$ ,  $x_{H2} = 30$ , P = 1 atm and T/T<sub>0</sub> = 1.



**Fig. 18.** LFS for NH<sub>3</sub>/ H<sub>2</sub>/O<sub>3</sub>/air mixtures at different  $x_{H2}$  and  $x_{O3}$ ,  $\phi = 1$ , P = 1 atm: a) T/T<sub>0</sub> = 1, b) T/T<sub>0</sub> = 1.5.

Figs. 17 and 18 present a surface plot depicting LFS for various  $NH_3/H_2/O_3/air$  blends across diverse conditions. This visualization effectively highlights the intricate relationships between flame characteristics and operational parameters, such as temperature, fuel-to-air ratio,  $O_3$ , and  $H_2$  concentration. Results show that incorporating a more reactive fuel component into  $NH_3$  such as  $H_2$  and  $O_3$  has a positive effect on the LFS. The addition of 0.01  $O_3$  in the oxidizer in terms of mole fractions has approximately the same effect as the addition of 10 %  $H_2$  on the LFS of  $NH_3/air$  mixture at normal conditions and the improvement of LFS is closely linked to  $O_3$  chemistry, especially fast exothermic ozonolysis reactions and the breakdown of  $O_3$  to form atomic oxygen.

## 5. Conclusion

In this study, an enhanced NH<sub>3</sub>/H<sub>2</sub>/Air mechanism was implemented and validated, and a comprehensive parametric analysis was performed. This analysis investigated the effects of various factors such as hydrogen (H<sub>2</sub>) concentrations, equivalence ratio ( $\Phi$ ), initial temperature, and initial pressure on laminar flame speed (LFS) and ignition delay time (IDT). Additionally, the impact of ozone (O<sub>3</sub>) concentration in the oxidizer, in terms of mole fraction ranging from 0 to 0.01, on the LFS of NH<sub>3</sub>/H<sub>2</sub>/air mixtures was examined. A significant aspect of the research involved the use of multi-gene genetic programming to accurately predict laminar flame speed under different fuel mixture conditions.

The key findings from this research are as follows:

- It was observed that LFS increases with the rise in  $H_2$  concentration and initial temperature. In contrast, an increase in initial pressure led to a decrease in LFS. Interestingly, at higher pressures (over 5 atmospheres), the effect of initial pressure on LFS lessens, and an optimized equivalence ratio, lying in the range of 1.10 - 1.20, is identified for achieving stable and efficient combustion.
- The study found that IDT decreases with an increase in  $H_2$  concentration, initial temperature, and initial pressure. However, at higher pressures (above 10 atmospheres), the influence of initial pressure on reducing IDT is less pronounced. For mixtures with 30 % and 50 %  $H_2$ , the study noted that IDTs could be shortened only at high temperatures (above 1200 K). At lower temperatures, IDTs tend to significantly increase, particularly as the higher  $H_2$  concentration leads to  $H_2$  chemistry dominating the ignition delays in the dual mixture.

- The addition of O<sub>3</sub> to the oxidizer, in mole fractions from 0 to 0.01, was also found to improve the LFS of the NH<sub>3</sub>/H<sub>2</sub>/air mixture under normal conditions. Adding 0.01 mol fraction of ozone to the oxidizer has approximately the same effect as adding 10 % hydrogen on the LFS of the NH<sub>3</sub>/air mixture at normal conditions.
- The predictive capability of the multi-gene genetic programming model developed in this study is promising. This was demonstrated through a comparison between the predicted values using the model and actual values obtained via chemkin simulations, showing a good agreement and confirming the model's accuracy for the examined test dataset.
- The results of this study provide useful insights for the application of numerical machine learning techniques in the field of zero-carbon combustion applications, indicating a significant stride forward in this area.

Looking ahead, there is immense potential for further development in this area. Future works could explore the incorporation of 3D Computational Fluid Dynamics (CFD) analysis simulations, which would provide a more detailed understanding of the combustion processes in green fuels. Such advancements could lead to even more efficient and environmentally friendly combustion technologies, reinforcing the role of green fuels in mitigating the effects of climate change and supporting the transition to a more sustainable energy future.

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#### CRediT authorship contribution statement

**Zubair Ali Shah:** Writing – original draft, Visualization, Software, Methodology, Data curation. **G. Marseglia:** Writing – review & editing, Writing – original draft, Investigation, Formal analysis. **M.G. De Giorgi:** Writing – original draft, Validation, Supervision, Software, Resources, Methodology, Conceptualization.

#### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Data availability

Data will be made available on request.

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